



## CO-COMBUSTION MODELING OF RICE HUSK AND PLASTIC BAG AS ENERGY SOURCE IN INDONESIA

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### ABSTRACT

This study was conducted to obtain a model combustion characteristics of rice husk and plastic bags as a energy source. The characteristics modeling using Autodesk Mechanical Desktop, Gambit, and Ansys - Fluent software. Maximum temperature of gas in the grate bed was obtained of about 1,710 K, in the furnace of about 1,670 K, and the average temperature in the furnace of about 1,086 K. The flue gas CO<sub>2</sub>, CO, and H<sub>2</sub>O in the furnace was obtained maximum of about 0.336% (3,360 ppm), 0.305% (3,050 ppm), and 0.132% (1,320 ppm), respectively. It was concluded that the co-combustion characteristics model of RH<sub>90</sub> + PB<sub>10</sub> produces temperature that meets the needs of a trap on the boiler and flue gas produces a small that is safe for the environment. Thus, it can be the basis for the development of utilization as fuel in the power plant.

**Keywords:** Co-combustion, modeling, rice husk, plastic bag, energy source.

### INTRODUCTION

Electrification ratio in Indonesia is still low, has reached an average of 72%. Even still there are four provinces, only around 20 - 40% (PT PLN - Persero, 2010). This shows the electric energy supply in Indonesia is still lacking. Rural communities there are still about 28% who do not use electric energy for everyday purposes. In urban areas also still frequent rolling blackouts. This is due to lack of power while electricity for the society and industry is increasing every year. In addition, fossil energy sources are a major source of power generation in Indonesia tend to be reduced drastic and cause environmental impacts. While the potential of rice husk and plastic waste in Indonesia is produced each year and has not been used as a source of energy, even still wasted as environmental pollution. Results of previous studies show Indonesia has a great potential of rice husk (RH) is about 13 294 × 106 tons, 13 151 × 106 tons, 13 809 × 106 tons in 2010, 2011, 2013 with an energy potential of approximately 51.696 GWh, 51.144 GWh, 53.702 GWh, respectively (Anshar *et al.*, 2014). This potential can be utilized as fuel in the power plant as well as the results of studies in Thailand (Madhiyanon *et al.*, 2009) and in India (Kapur *et al.*, 1996).

In addition, the potential of municipal solid waste (MSW) and plastic solid waste (PSW) are also available on each province produced every day in urban areas (Anshar *et al.*, 2015c, 2015b). This potential is wasted as waste that pollutes the environment. This study was conducted to obtain characteristics model of co-combustion of rice husks and plastic bags as an alternative energy source at the power plant in Indonesia. Modeling results are expected to contribute to further research and for policy-makers in the development and the waste as a source of electric energy in Indonesia.

### GEOMETRY MODEL OF FURNACE AND BOUNDARY CONDITION

This modeling using the boundary condition namely: fuel feed rate of about 6,575 kg/h at 298 K, the overall air/fuel stoichiometric ratio of about 0.84, the primary water about 6 kg/s at 453 K, the secondary air 1 and 2 of about 3.2 kg/s at temperatures around 453 K. Geometry of the furnace and the type of boundary condition are used: inlet velocity, mass flow inlet, wall and outflow. Meshing is made with a quad element, pave type, size interval, spacing about 0:05. A total mesh consists of about 28,875 nodes and 28,434 elements to generate proper combustion models. Geometry models of furnaces are used for small power plants i.e. 7.5 × 5.7 × 12 m is presented in Figure-1. Co-combustion modeling of RH and plastic bags (PB) performed with a ratio between 90% of RH and 10% of PB (RH<sub>90</sub>+PB<sub>10</sub>). Testing the calorific value (CV) is performed by using a bomb calorimeter by standard procedure ASTM D.5865. Proximate analysis was carried out under the standard procedure ASTM D 3172 - 3175 and ISO 565. While, the ultimate analysis was performed under the standard procedure ASTM D 3176, ASTM D 4239, and ASTM D 5373. This method is in line with previous studies studies (Maiti *et al.*, 2006 ; Patel and Kumar, 2009). Furnace geometry is obtained by using Autodesk Mechanical Desktop software. Furnace geometry is obtained by using Autodesk Mechanical Desktop software. Mashing is done with Gambit software, and modeling co-combustion (RH<sub>90</sub>+PB<sub>10</sub>) was performed using Ansys - Fluent software. Boundary condition is determined based on the capacity output of energy that will be generated by reference to some previous study (Kær, 2004; Kær, 2005; Husain *et al.*, 2006; Yin *et al.*, 2012; Shin *et al.*, 2013; Anshar *et al.*, 2015a).



## TRANSPORT AND COMBUSTION REACTION EQUATIONS

Biomass combustion on grate bed furnace is basically divided into two parts, namely in-grate bed and over-grate bed combustion. In biomass combustion on the grate bed furnace occurred heat and mass exchange between the solid phase and the gas phase. The change of the solid phase into the gas phase occurs in grate bed due to the combustion while the gas phase occurs in over grate bed combustion chamber as a result of combustion. Scheme numerically solving the combustion process is obtained by using a computer program (Yang *et al.*, 2007; Yu *et al.*, 2010). The conservation equations for solid phase and gas phase in grate bed are as follows:

Continuity equation:

$$\frac{\partial \rho_{sb}}{\partial t} + U_b \frac{\partial \rho_{sb}}{\partial x} + \frac{\partial (\rho_{sb} V_s)}{\partial y} = -S_s \quad (1)$$

Energy equation:

$$\begin{aligned} & \frac{\partial (\rho_{sb} H_s)}{\partial t} + U_b \frac{\partial (\rho_{sb} H_s)}{\partial x} + \frac{\partial (\rho_{sb} V_s H_s)}{\partial y} \\ & = \frac{\partial}{\partial x} \left( \lambda_s \frac{\partial T_s}{\partial x} \right) + \frac{\partial}{\partial y} \left( \lambda_s \frac{\partial T_s}{\partial y} \right) - S_s h_s (T_s - T_g) + \sum \Delta h_k \end{aligned} \quad (2)$$

Species equation:

$$\begin{aligned} & \frac{\partial (\rho_{sb} Y_{si})}{\partial t} + U_b \frac{\partial (\rho_{sb} Y_{si})}{\partial x} + \frac{\partial (\rho_{sb} V_s Y_{si})}{\partial y} \\ & = \frac{\partial}{\partial x} \left( D_s \frac{\partial (\rho_{sb} Y_{si})}{\partial x} \right) + \frac{\partial}{\partial y} \left( D_s \frac{\partial (\rho_{sb} Y_{si})}{\partial y} \right) - S_{si} \end{aligned} \quad (3)$$

The resultant conservation equations for gas phase in grate bed as follows:

Continuity equation:

$$\frac{\partial (\phi \rho_g)}{\partial t} + \frac{\partial (\phi \rho_g U_g)}{\partial x} + \frac{\partial (\phi \rho_g V_g)}{\partial y} = S_g \quad (4)$$

Energy equation:

$$\begin{aligned} & \frac{\partial (\phi \rho_g H_g)}{\partial t} + \frac{\partial (\phi \rho_g U_g H_g)}{\partial x} + \frac{\partial (\phi \rho_g V_g H_g)}{\partial y} \\ & = \frac{\partial}{\partial x} \left( \lambda_g \frac{\partial T_g}{\partial x} \right) + \frac{\partial}{\partial y} \left( \lambda_g \frac{\partial T_g}{\partial y} \right) + S_g h_s (T_s - T_g) + \sum \Delta h_k \end{aligned} \quad (5)$$

Species equation:

$$\begin{aligned} & \frac{\partial (\phi \rho_g Y_{gj})}{\partial t} + \frac{\partial (\phi \rho_g U_g Y_{gj})}{\partial x} + \frac{\partial (\phi \rho_g V_g Y_{gj})}{\partial y} \\ & = \frac{\partial}{\partial x} \left( D_g \frac{\partial (\phi \rho_g Y_{gj})}{\partial x} \right) + \frac{\partial}{\partial y} \left( D_g \frac{\partial (\phi \rho_g Y_{gj})}{\partial y} \right) + S_{gj} + S_{gj} \end{aligned} \quad (6)$$

Where  $D$  = mass diffusion coefficients,  $m^2/s$ ,  $H$  = enthalpy,  $J/kg$ ,  $h_s$  = convective mass transfer coefficient

between solid and gas,  $m/s$ ,  $h_s$  = convective heat transfer coefficient between solid and gas,  $W/m^2 K$ ,  $\Delta h_k$  = heat effect for  $k$ th process or reaction,  $W/m^3$ ,  $S$  = mass source term,  $kg/m^3 s$ ,  $S_a$  = particle surface area,  $m^2$ ,  $t$  = time,  $s$ ,  $T$  = temperature,  $K$ ,  $U$  = horizontal velocity,  $m/s$ ,  $V$  = vertical velocity,  $m/s$ ,  $x$  = co-ordinate in the direction of grate length,  $m$ ,  $X$  = solid mass loss fraction, mass fraction of pollutants,  $y$  = co-ordinate in the direction of bed height,  $m$ ,  $Y$  = mass fraction of species,  $\rho$  = density,  $kg/m^3$ ,  $\lambda$  = thermal conductivity,  $W/m K^{-1}$ ,  $\phi$  = void fraction in the bed,  $S_s$  = mass loss rate from solid ( $S_s = Revp + RV + RC$ ),  $kg/m^3 s$ ,  $k$  = kinetic rate of reactions. Subscripts  $b$  = bed,  $g$  = gas,  $i$  = species in solid, i.e., moisture, volatile matter, fixed carbon and ash,  $j$  = species in gas, i.e.,  $O_2$ ,  $CO_2$ ,  $CO$ ,  $NH_3$ ,  $NO$ ,  $N_2$ ,  $H_2$ ,  $CH_4$  and  $H_2O$ ,  $s$  = solid,  $sb$  = bulk density,

## RESULTS AND DISCUSSIONS

### Input data of co-combustion modeling

Input data for co-combustion modeling of  $RH_{90+PB_{10}}$  and  $RH$  is to use the result data of proximate and ultimate analysis, as presented in Table-1. In this case,  $RH$  modeling performed as a comparison of co-combustion modeling of  $RH_{90+PB_{10}}$ . The analysis showed the addition of approximately 10%  $PB$  in the  $RH$  increase the calorific value (CV), volatile matter (VM), carbon (C), water vapor ( $H_2O$ ). In addition, the lower the moisture content (MC), fixed carbon (FC), oxygen (O), nitrogen (N), and ash. This means that the co-combustion  $RH_{90+PB_{10}}$  can improve fuel quality of  $RH$ .

**Table-1.** Proximate and ultimate analysis of  $RH_{90+PB_{10}}$  and  $RH$ .

Modeling parameter input	$RH_{90+PB_{10}}$	$RH$
CV (kJ/kg)	18,847	13,442
FC (%)	13.62	14.81
VM (%)	58.65	55.62
MC (%)	9.68	10.46
C (%)	42.21	39.28
H (%)	5.82	5.08
O (%)	33.45	35.81
N (%)	0.38	0.64
S (%)	0.09	0.08
Ash (%)	18.05	19.11

Co-combustion modeling results of  $RH_{90+PB_{10}}$  in grate bed furnace showed that the co-combustion provide a significant influence on several of co-combustion parameter. In this case, increase gas temperature ( $T_g$ ), increase the combustion gas velocity ( $V_g$ ), and increase the total energy in the fuel input. Overall air fuel ratio (AFR) stoichiomertri decreases which means less air needs, but solid gasification efficiency is complete



(100%). Some parameters of co-combustion modeling results of RH<sub>90</sub>+PB<sub>10</sub> has similarities with the modeling parameters result of RH, but differ significantly in

temperature, total energy input, and overall AFR. Modeling parameter result are presented in Table-2.

**Table-2.** Modeling parameter results of RH<sub>90</sub>+PB<sub>10</sub> and RH on grate bed furnace.

Modeling parameter results	RH <sub>90</sub> +PB <sub>10</sub>	RH
Teotitcal air (Nm <sup>3</sup> /kg waste	3.73	3.23
Total primary air (Nm <sup>3</sup> /min)	296.19	296.19
Final carbon in solid (% mass)	8.4e-096	8.4e-096
Solid gasification efficiency (%)	100	100
Moisture evaporated (kg/hr)	638.26	694.99
Volatile released (kg/hr)	3,495.4	3,584.3
Total mass loss (kg/hr)	5,018.1	5,259.8
Tg max.(K)	1,710	1,680
Tg Average (K)	1,186	1,138
Tg exit (K)	1100	950
Vg (m/s)	9	8.51
Overall AFR	0.726	0.837
Fuel input (kg/h)	6,575.35	6,575.35
Energy in fuel input (MWt)	34.42	24.55

Co-combustion modeling of RH<sub>90</sub>+PB<sub>10</sub> and temperature distribution in the grate bed furnace is presented in Figure-2. In this case, the combustion process began to take place at a distance of 0.4 m from the fuel input, but the burning began to stabilize in the range of 0.8 - 6.2 m with a temperature of about 969 – 1,710 K. After that, the temperature began to decrease until it reaches temperatures of 454 K, which occurs the decrease in temperature of bottom ash.

Figure-3 shows the combustion start occurs at a distance of 0.4 m from the fuel input where CO, CO<sub>2</sub>, H<sub>2</sub>O increase and fluctuate. At a distance of 2.3 m, H<sub>2</sub>O to zero, which means all the water content in RH<sub>90</sub>+PB<sub>10</sub> turn into gas phase. At a distance of 3.7 m, CO and CO<sub>2</sub> to zero. In these conditions RH<sub>90</sub>+PB<sub>10</sub> already burn completely so as not to form more CO<sub>2</sub>, CO, and H<sub>2</sub>O. In these conditions the CO and CO<sub>2</sub> reaches zero, while O<sub>2</sub> drastically increase reaching normal condition (21%). On top of the bed (over-bed) combustion temperature distribution is very uneven due to the gases do not burn completely.

In addition, Figure-4 shows the mass loss rate, volatile release, moisture evaporation, and char burning rate occurred fluctuation start at a distance of 0.4 m to 1.87 m from the fuel inlet. Volatile release is proportional to the mass loss rate, which release volatile increases when the mass loss rate increases. This suggests that volatile release occurs due to the mass loss caused by the heating and combustion processes. The maximum value of mass loss rate and the volatile release reached 827.7 kg / m<sup>2</sup> h at a distance of about 1.8 m from the fuel inlet. At a distance of 0.4 -1.87 m, moisture evaporation process also occurs. After the evaporation of moisture, volatile release, and the mass loss rate is over, there will be a process maximal char burning rate at 0.4-3.7 m area until the end.

In these conditions, volatile release dramatically decreases until it reaches zero, while the char burning rate

reaches zero at a distance of 3.7 m from the fuel inlet. The process of burning rice husk and plastic bag in the bed take place starting at a distance of approximately 0.4 m to 7.66 m. Co-combustion model characteristics of rice husk and the plastic bag has similarities with the characteristics model of previous studies (Ryu *et al.*, 2005; Yang *et al.*, 2007), although the value of each variable is different because differences in input data and boundary conditions in the combustion process.

Figure-5 shows the characteristics of the combustion gas and gas temperature in the furnace. Gases of combustion in the grate bed followed the combustion in the furnace by adding secondary air so that gases of combustion burn completely before exiting the furnace. The maximum temperature at the base of the furnace is about 1670 K and 1100 K furnace exit. At the base of the furnace obtain CO maximum of about 0.305% (3050 ppm), CO<sub>2</sub> maximum of about 0.336% (3360 ppm), and H<sub>2</sub>O maximum of about 0.132% (1320 ppm). These conditions indicate that the co-combustion RH<sub>90</sub>+PB<sub>10</sub> meet feasibility as fuel in the power plant because it produces gas temperature that meets the needs of the boiler and exhaust gas are small so no impact on the environment.

Co-combustion modeling result of RH<sub>90</sub>+PB<sub>10</sub> in grate bed furnace show that co-combustion of RH<sub>90</sub>+PB<sub>10</sub> provide a significant influence on several combustion parameters. In this case, increase of maximum gas temperature, average temperature, exit temperature, increase the combustion gas velocity, and increase the total energy in the fuel input. However, moisture evaporated, volatile released, and total mass loss decrease. This shows that the water content in the fuel RH<sub>90</sub> + PB<sub>10</sub> is smaller than the water content of the RH. Thus, the combustion air requirements (AFR stoichiomertri) in the fuel RH<sub>90</sub> + PB<sub>10</sub> are reduced.

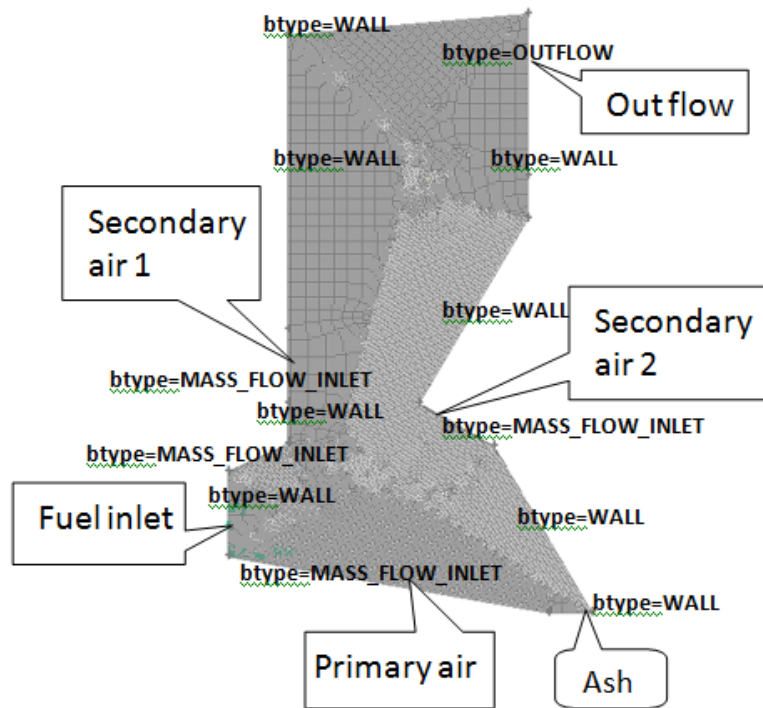


Figure-1. Geometry of grate bed furnace.

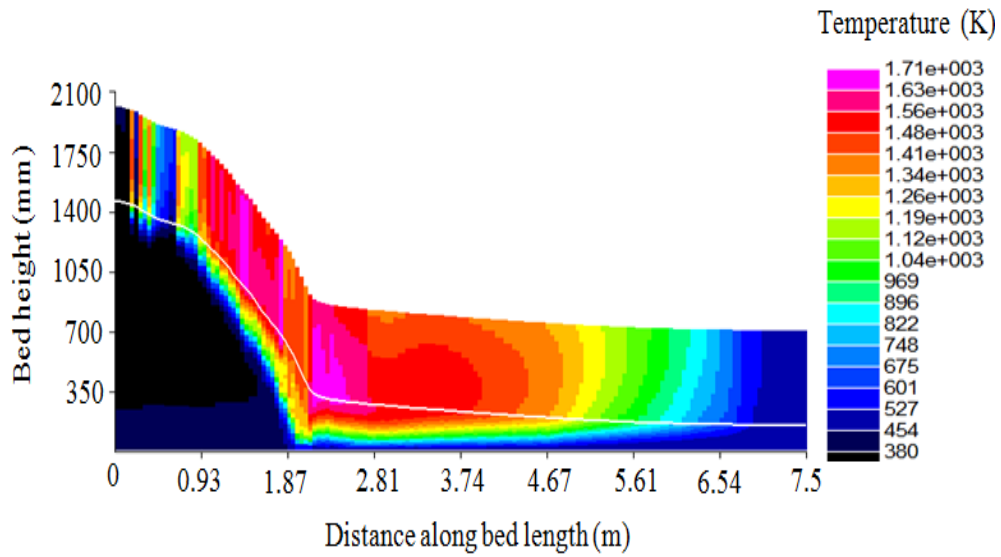
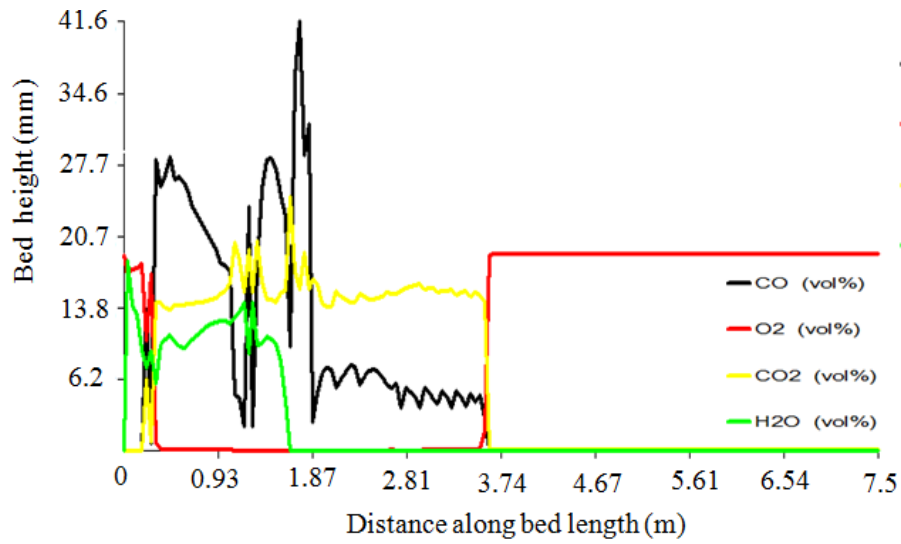
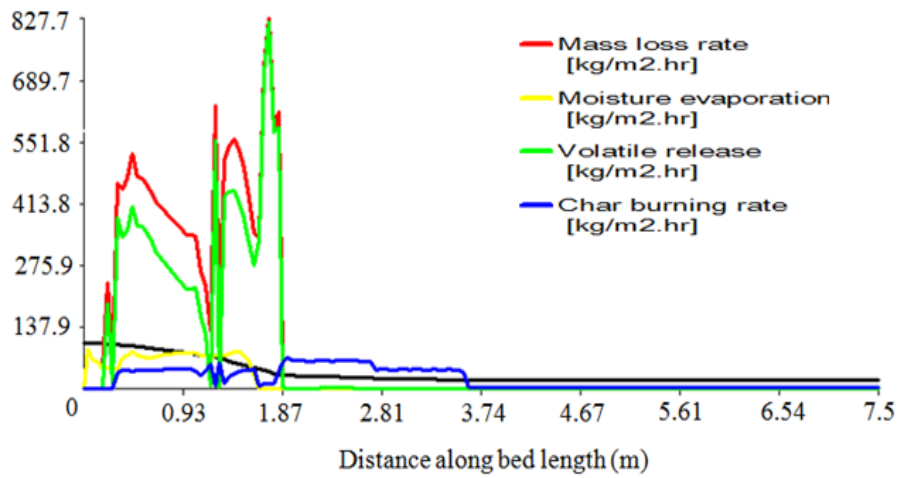


Figure-2. Gas temperature characteristic of  $RH_{90}+PB_{10}$  in grate bed.

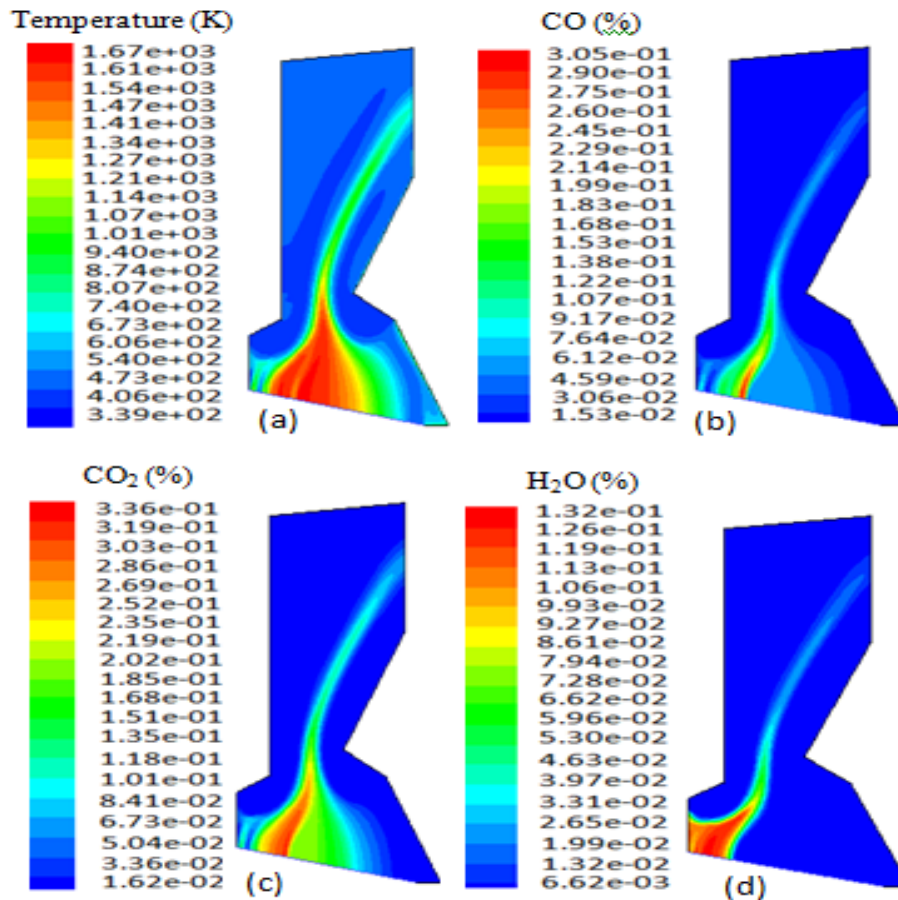


**Figure-3.** Profile of CO, CO<sub>2</sub>, O<sub>2</sub>, and H<sub>2</sub>O of RH<sub>90</sub>+PB<sub>10</sub> at the top bed.



**Figure-4.** Profile of combustion gas of RH<sub>90</sub>+PB<sub>10</sub> at the top bed.





**Figure-5.** Contours of of RH<sub>90</sub>+PB<sub>10</sub>: a) Static temperature (K); b) CO (%); c) CO<sub>2</sub> (%); d) H<sub>2</sub>O (%).

## CONCLUSIONS

Co-combustion model characteristics of RH<sub>90</sub>+PB<sub>10</sub> meet feasibility as fuel in the power plant because it produces gas temperature that meets the needs of the boiler temperature. In addition, the exhaust gas is low. Maximum temperature on the grate bed of about 1710 K, the maximum temperature in the furnace gas of about 1670 K, and the average temperature of about 1086 K. The flue gas CO<sub>2</sub>, CO, and H<sub>2</sub>O in the furnace obtained maximum of about 0.336% (3360 ppm), 0.305% (3050 ppm), and 0.132% (1320 ppm), respectively. Thus, it can be a reference for the development of utilization as fuel in the power plant in Indonesia.

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